

Estimation of Refrigeration side Heat transfer coefficient of Zero Ozone Depletion Refrigerant R134a used in Mobile AC in comparison with R22 Refrigerant

Kasuba Sainath

*Research scholar JNTUH & Asso. professor in MED
Sreyas Institute of Engineering and Technology
Nagole, Hyderabad. India 500068.,*

P.S.Ravi

Research scholar OU Hyderabad,

Rajan Saini

*Student of MED,
Sreyas Institute of Engineering & Technology,
Nagole, Hyderabad.*

Dr Suresh Akella

*Principal & professor in MED
Sreyas Institute of Engineering and Technology
Nagole, Hyderabad. India 500068.,*

Abstract- This document presents a theoretical study, Design & Experimental results gives the performance of R134a refrigerant as alternative to ozone layer depleting R22 refrigerant. R134a refrigerant has no ozone layer depleting property and inconsequential global warming potential with respect to R22. As per the rules of Montreal and Kyoto protocol the world community has decided to reduce the production and consumption of HCFC-22 from the refrigeration and air conditioning industry completely by 2020. In R22, chlorine is the element which depletes the Ozone layer, with Ozone Depletion Potential 0.05 and Global Warming Potential 1700, which effects the environment

Keywords –ODP, GWP, Critical pressure, critical pressure, Enthalpy, C.O.P, condenser, rotary compressor, refrigerants, R22, R134a, capillary tube, thermal conductivity, heat transfer.

I. INTRODUCTION

The purpose of this study was to compare R22 and R134a refrigerants on the basis of their environmental affect and thermal properties. The objective of this study is to show how R22 can be replaced by R134a as this refrigerant has better coefficient of performance than R22. Relatively, this study was motivated by Montreal Protocol, an international agreement by many nations to reduce the production of ozone-depleting substances. Since then, there are many experiments carries forward and much discussion about alternative refrigerants.

This report discuss about the calculations of R134a and R22 refrigerants. It also shows the thermal properties of both the refrigerants. It also shows the p-h diagram and concluded by the overall properties of both the refrigerants.

II. AIR CONDITIONING SYSTEM

Before learning the operation of the air-conditioner system, we should know first about the significant components which they are applied in the refrigerant circulate system.

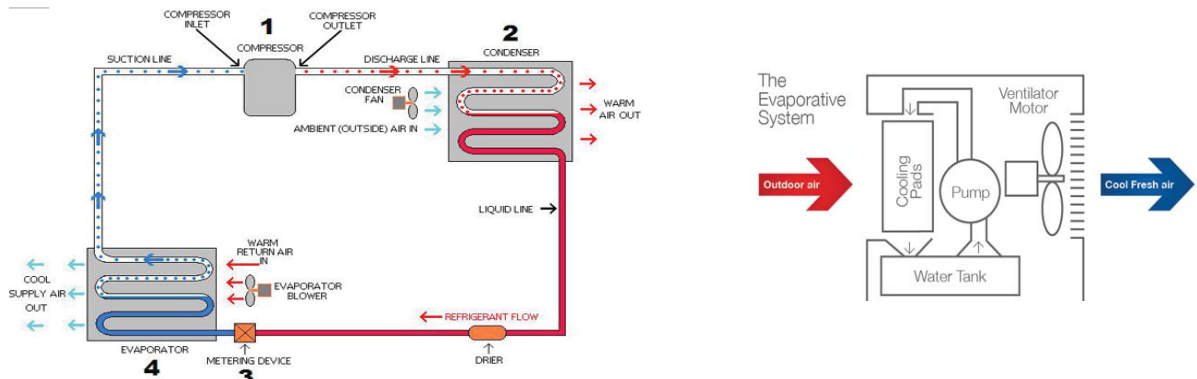


Fig1. Refrigerant flow of Air Conditioning System & Working of the Air Cooler

Compressor: It drives the refrigerant flow into each part of the air-conditioner so these caused the temperature and the air pressure in the refrigerant being high.

Condenser: It drains heat from the refrigerant.

Evaporator: It can absorb and transfer the heat in the building to the refrigerant.

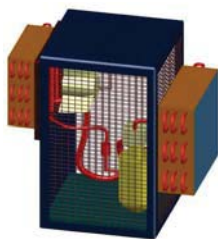
Throttling Device: It reduces the air pressure and the temperature in the refrigerant. Generally, it can be used as Capillary tube or Expansion Valve.

The cooling system as mentioned above is Vapor-Compression Circulate system which it has the simply working regulation via driving the refrigerant flow along the system and this also passed continually throughout 4 major components as Refrigerant Circulate system. Besides, the followings are its working process.

1. Firstly, the compressor will absorb and charge the refrigerant for enhancing its pressure and temperature and also move it forward to the evaporator later.
2. Then, the refrigerant will be flown throughout the evaporator by using the fan drain the heat out. So it caused the refrigerant's temperature in the evaporator which it is emanating being low. Next, this will be flushed to Throttling Device hereafter.
3. Next, the pressure and temperature in the refrigerant that flown through Throttling Device will be quite low. After that, it will be flushed into the cooling coil
4. Later, the refrigerant will be circulated around the cooling coil which it used the fan to absorb heating in that room so it caused the room's temperature getting low and the refrigerant's temperature of emanating cooling coil getting high (stable pressure). Lastly, this refrigerant will be transferred back to the compressor for operating over circulated system continually

III. DESIGN OF A MOBILE AIR CONDITIONER

Design of a mobile air conditioner is done using AutoCAD 3D. The parts of air conditioner are compressor, condenser, evaporator, capillary tube and cooler fan.



S. No	Description	Specification
1	Model	pH170G1C-3DZDU2
2	Display. (cm ³ /rev)	16.8
3	Capacity (W)	3420
4	Capacity (BTU/h)	11670
5	Power (W)	1085
6	COP (W/W)	3.15
7	Capacitor(F/V)	35/370

Fig2. 3D Design Of Air Conditioner Toshiba / GMCC R22 1 -60Hz-208/230V air conditioner rotary compressor

Tube and fin Condenser:

It consists of a copper coil located in a steel rectangular shell, alternatively placed, bent in U shape and brazed. Water is circulated through the coil, and refrigerant vapors are discharged from the compressor, heat exchange takes place between the water and the refrigerant, with same pressure temperature drops on copper tubes.

Though it's economical, this type of condensers maintenance is difficult and also if any leakage occurs entire unit is to be replaced.

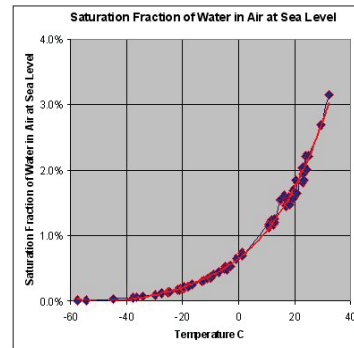


Fig3. Condenser attached behind the cooler; Relationship To Human Control

Dew point		Human perception[2]	Relative humidity at 32 °C (90 °F)
Over 26 °C	Over 80 °F	Severely high. Even deadly for Bronchitis	65% and higher
24–26 °C	75–80 °F	Extremely uncomfortable, fairly oppressive	62%
21–24 °C	70–74 °F	Very humid, quite uneasy	52–60%
18–21 °C	65–69 °F	Somewhat uneasy for most people at upper edge	44–52%
16–18 °C	60–64 °F	OK for most, but all the humidity at upper edge	37–46%
13–16 °C	55–59 °F	Comfortable	38–41%
10–12 °C	50–54 °F	Very comfortable	31–37%
Under 10 °C	Under 50 °F	A bit dry for some	30% and lower

Fig 4. Relationship to Human Control

IV. CALCULATIONS OF R134A REFRIGERANT

Design parameters:

- Capacity of air conditioner $1\frac{1}{2} + R = 1.5 * 210 \text{ KJ/min} = 1.5 * 210 * \frac{60}{60} \text{ J/sec} = 5250 \text{ W}$
- Roll bond tube outside diameter $d_o = \frac{1}{8} = 12.7 \text{ mm}$
- Thickness of tube = 2.108mm
- Inside diameter of tube $d_i = d_o - 2t = 8.484 \text{ mm}$
- $T_{\text{condenser}} = 50^{\circ}\text{C}$ $T_{\text{evap}} = 5^{\circ}\text{C}$
- $P_{\text{cond}} = 13.77 \text{ bar}$ $P_{\text{evap}} = 3.49705 \text{ bar} = 3.49705 \text{ bar}$

Basic Cycle Calculations

1. Assumptions

- There is no liquid sub cooling
- Vapour super heat at evaporator is ok

2. Mass flow rate Calculations

From Ref prop, $h_1 = 401.57 \text{ KJ/kg} = 401.57 * 10^3 \text{ J/kg}$ $h_3 = h_4 = 271.59 \text{ KJ/kg} = 271.59 * 10^3 \text{ J/kg}$
 $m(h_1 - h_4) = 5250 \text{ W}$ $m(401.57 - 271.59) * 10^3 = 5250$ $m = 0.0404 \text{ Kg/sec}$

- Finding quality of refrigerant at entry of roll band evaporator

For Isenthalpic flow $h_3 = h_4$ $h_3 = (h_f + xh_{fg})_4$
 $h_{32} = h_{f3} = 271.59 \text{ KJ/kg}$ $h_{f4} = 206.725 \text{ KJ/kg}$ $(h_{fg})_4 = 195.98 \text{ KJ/kg}$
 $271.59 = 206.725 + x(195.98)$ $x = 0.331$ therefore, quantity of refrigerant, $x_4 = 0.331$

- Porkel, Qumstan, Spilter condition for F134a (ASHRAE)

$$\frac{h}{K} = C_1 \left[\left(\frac{P}{P_c} \right)^2 \left(\frac{h_{fg}}{h_g} \right) \right]^n$$

Where, h= internal (Refrigerant side heat transfer coefficient)

D= internal diameter of tube
 K= thermal conductivity refrigerant
 $C_1 = \text{constant} = 9 \times 10^{-4}$ if $x \leq 0.9$ $= 8.2 \times 10^{-3}$ if $x \geq 1.0$, x is quantity refrigerant leaving roll bond evaporator
 $n = \text{constant} = 0.5$ if $x < 0.9$ $= 0.4$ if $x \geq 1.0$
 $\mu_L = \text{viscosity of refrigerant R134a at } 5^\circ\text{C}$
 J= Joule coefficient= 1 for SI unit

$$\Delta h_{fg} = (1 - 0.9851)(198.99) = 131.11 \text{ KJ/kg}$$

$$K_1 = 91.46 \times 10^{-3} \text{ W/mK (from Ref Prop)}$$

G= mass velocity of refrigerant = m/A

$$A = \frac{\pi}{4}(d_i)^2 = \frac{\pi}{4}(8.484 \times 10^{-3})^2 = 5.653 \times 10^{-5} \text{ m}^2$$

$$G = \frac{0.001}{5.653 \times 10^{-5}} = 714.64 \text{ Kg/Sm}^2$$

$$G_c = 1$$

Total length of roll band evaporator tube= 80m

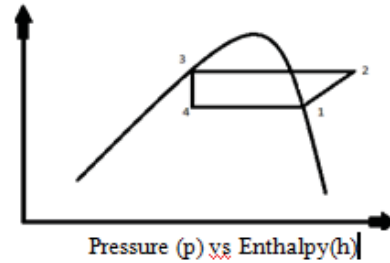
If 8 pannels are used length of evaporator tube in each pannel will be $\frac{80}{8} = 10\text{m}$, number of pannel= 10, length of pannel= 1m

If 8 pannels are kept parallel for each other, the length of tube per pannel will be $8 \times 1 = 8\text{m}$.

$\mu_L = 249.9 \times 10^{-6} \text{ pas (From Ref Prop)}$

$$\frac{0.1348 \times 10^{-4}}{714.64 \times 10^{-4}} = 8.2 \times 10^{-3} \left[\left\{ \frac{714.64 \times 8.484 \times 10^{-3}}{249.9 \times 10^{-6}} \right\}^2 \times \left[\frac{131.11 \times 10^3}{714.64} \right]^{0.4} \right] h = 5540.29 \text{ W/m}^2\text{K}$$

Therefore, Inside HT coefficient for R134a is $5540.29 \text{ W/m}^2\text{K}$



V. CALCULATIONS OF R22 REFRIGERANT

Design parameters:

- Capacity of air conditioner $1 \frac{1}{2} + R = 1.5 \times 210 \text{ KJ/min} = 1.5 \times 210 \times \frac{1000}{60} \text{ J/sec} = 5250 \text{ W}$
- Roll bond tube outside diameter $d_o = \frac{1}{8} = 12.7\text{mm}$
- Thickness of tube = 2.108mm
- Inside diameter of tube $d_i = d_o - 2t = 8.484\text{mm}$
- $T_{\text{condenser}} = 50^\circ\text{C}$ $T_{\text{evap}} = 5^\circ\text{C}$

Basic Cycle Calculations

1. Assumptions

- There is no liquid sub cooling
- Vapour super heat at evaporator is ok

2. Mass flow rate calculations

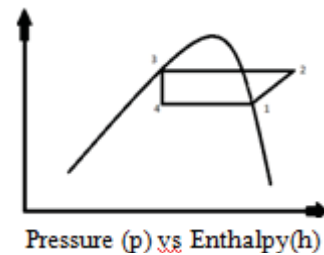
From REFPROP, For Refrigerant R-22 properties, enthalpies at state 1 and state 4 are 407.45 kJ/kg and 262.27 kJ/kg respectively.

The mass flow rate is calculated from the relation $m (h_1 - h_4) = \text{heat load}$.

The estimated mass flow rate of refrigerant is $m = 0.03616 \text{ kg s}^{-1}$

The heat transfer coefficient so calculated for R-22 is $1244.38 \text{ W/m}^2\text{K}$

- Dittus Boelter equation: The heat transfer coefficient so calculated for R-22 is $1236.46 \text{ W/m}^2\text{K}$
 Nusselt's number $Nu = 0.023 Re^{0.8} Pr^{0.4}$ Nusselt's number is given by $Nu = (h d)/k$
- Correlation from heat transfer data book: The heat transfer coefficient so calculated for R-22 is $1299.31 \text{ W/m}^2\text{K}$
 Nusselt's number $Nu = 0.026 Re^{0.8} Pr^{(1/3)}$
- Gnielinski equation: The heat transfer coefficient so calculated for R-22 is $1175.25 \text{ W/m}^2\text{K}$
 $Nud = \{ (f/8) \times (Re - 1000) Pr \} / \{ 1 + 12.7 (f/8)^{0.5} (Pr/3) \}$ friction factor, $f = (0.79 \ln Re - 1.164) - 2$

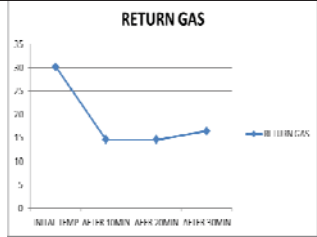
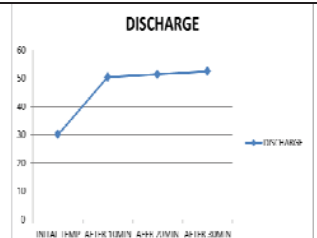
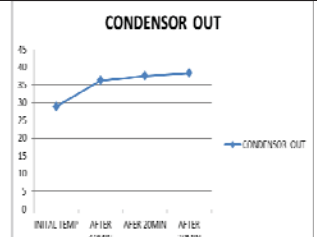
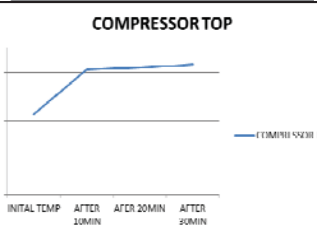


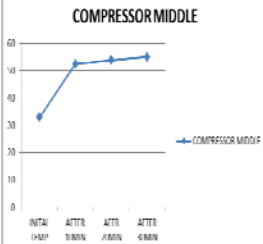
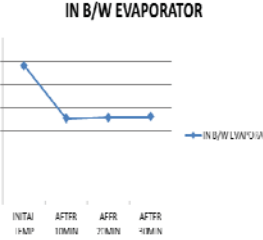
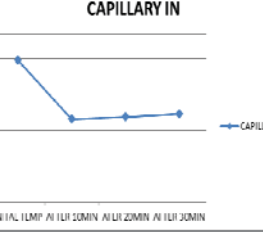
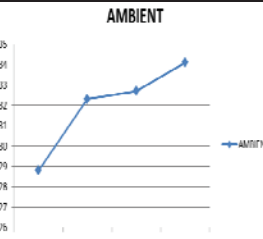

VI. RESULTS & CONCLUSION

In the present work we have identified there are 11 critical areas where all these conditions play a vital role in the present specified application, from the cooling effect of modified air cooler. The 11 critical thermocouples results identified are as shown below

S.no		Initial temp	After 10min	Afer 20min	After 30min
1	Return gas	30.2	14.6	14.6	16.5
2	Discharge	30.1	50.4	51.3	52.4
3	Condensor out	28.9	36.3	37.5	38.3
4	Compressor top	32.8	51.3	52.2	53.1
5	Compressor middle	32.9	52.5	53.9	55
6	Capillary in	29.6	17.3	17.8	18.4
7	In b/w evaporator	29.0	17.7	17.9	18.1
8	Evaporator out	28.9	16.7	17.1	17.8
9	Ambient	28.8	32.3	32.7	34.1
10	Wet-bulb temperture	30	30	31	32
11	Dry-bulb temerature	32	32	35	35

The following results are explained in detail with the results obtained by the thermo couples as follows below

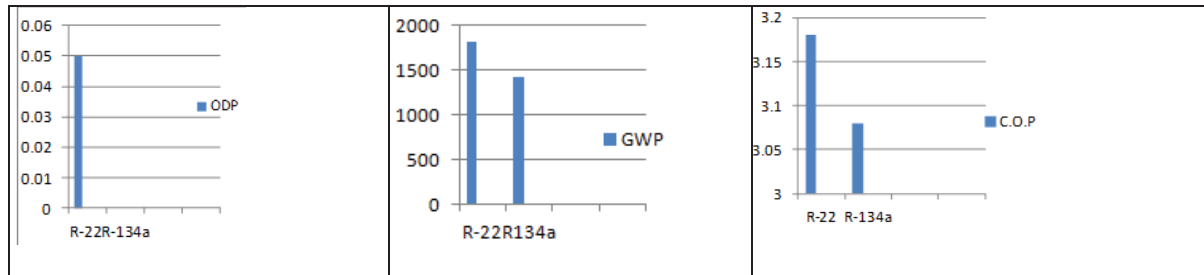
<p>Graph 1 shows the return gas temperature from compressor that are measured at four stages 1. Initial temp 2. After 10 minutes 3. After 20 minutes 4. After 30 minutes. The initial temperature of the gas from the compressor, at initial condition the temp is 30.2, after 10 minutes the temp is 14.6, after 20 minutes the temp is 14.6 and after 30 minutes the temp is 16.5</p>	
<p>Graph 2 shows the discharge temperature of refrigerant that are measured at four stages 1. Initial temp 2. After 10 minutes 3. After 20 minutes 4. After 30 minutes. The initial temperature of the discharge temperature of refrigerant, at initial condition the temp is 30.1, after 10 minutes the temp is 50.4, after 20 minutes the temp is 51.3 and after 30 minutes the temp is 52.4.</p>	
<p>Graph 3 shows the temperatures of the condenser out are measured at four stages 1. Initial temp 2. After 10 minutes 3. After 20 minutes 4. After 30 minutes. The initial temperature of the condenser out is, at initial condition the temp is 28.9, after 10 minutes the temp is 36.3, after 20 minutes the temp is 37.5 and after 30 minutes the temp is 38.3.</p>	
<p>Graph 4 shows the temperature of the compressor top are measured at four conditions 1. Initial temp 2. After 10 minutes 3. After 20 minutes 4. After 30 minutes. The initial temperature of the compressor top is, at initial condition the temp is 32.8, after 10 minutes the temp is 51.3, after 20 minutes the temp is 52.2 and after 30 minutes the temp is 53.1.</p>	

<p>Graph 5 shows the temperature of the compressor middle are measured at four conditions 1. Initial temp 2. After 10 mints 3. After 20 mints 4. After 30 mints.The initial temperature of thecompressor middle, at initial condition the temp is 2.9,after 10 mints the temp is 52.5,after 20 mints the temp is 53.9 and after 30 mints the temp is 55.</p>	 <table border="1"> <caption>COMPRESSOR MIDDLE</caption> <thead> <tr> <th>Condition</th> <th>Temperature</th> </tr> </thead> <tbody> <tr> <td>INITIAL</td> <td>2.9</td> </tr> <tr> <td>AFTER 10MIN</td> <td>52.5</td> </tr> <tr> <td>AFTER 20MIN</td> <td>53.9</td> </tr> <tr> <td>AFTER 30MIN</td> <td>55</td> </tr> </tbody> </table>	Condition	Temperature	INITIAL	2.9	AFTER 10MIN	52.5	AFTER 20MIN	53.9	AFTER 30MIN	55
Condition	Temperature										
INITIAL	2.9										
AFTER 10MIN	52.5										
AFTER 20MIN	53.9										
AFTER 30MIN	55										
<p>Graph 6 shows the temperature in between evaporator are measured at four stages 1. Initial temp 2. After 10 minutes 3. After 20 minutes 4. After 30 minutes.The initial temperature of in between evaporator, at initial condition the temp is 29.0,after 10 minutes the temp is 17.7,after 20 minutes the temp is 17.9 and after 30 minutes the temp is 18.1.</p>	 <table border="1"> <caption>IN B/W EVAPORATOR</caption> <thead> <tr> <th>Condition</th> <th>Temperature</th> </tr> </thead> <tbody> <tr> <td>INITIAL</td> <td>29.0</td> </tr> <tr> <td>AFTER 10MIN</td> <td>17.7</td> </tr> <tr> <td>AFTER 20MIN</td> <td>17.9</td> </tr> <tr> <td>AFTER 30MIN</td> <td>18.1</td> </tr> </tbody> </table>	Condition	Temperature	INITIAL	29.0	AFTER 10MIN	17.7	AFTER 20MIN	17.9	AFTER 30MIN	18.1
Condition	Temperature										
INITIAL	29.0										
AFTER 10MIN	17.7										
AFTER 20MIN	17.9										
AFTER 30MIN	18.1										
<p>Graph 7 shows the temperature of capillary in are measured at four stages1. Initial temp 2. After 10 minutes 3. After 20 minutes 4. After 30 minutes.The initial temperature of the capilary in is , at initial condition the temp is 29.6,after 10 minutes the temp is 17.3,after 20 minutes the temp is 17.8 and after 30 minutes the temp is 18.4.</p>	 <table border="1"> <caption>CAPILLARY IN</caption> <thead> <tr> <th>Condition</th> <th>Temperature</th> </tr> </thead> <tbody> <tr> <td>INITIAL</td> <td>29.6</td> </tr> <tr> <td>AFTER 10MIN</td> <td>17.3</td> </tr> <tr> <td>AFTER 20MIN</td> <td>17.8</td> </tr> <tr> <td>AFTER 30MIN</td> <td>18.4</td> </tr> </tbody> </table>	Condition	Temperature	INITIAL	29.6	AFTER 10MIN	17.3	AFTER 20MIN	17.8	AFTER 30MIN	18.4
Condition	Temperature										
INITIAL	29.6										
AFTER 10MIN	17.3										
AFTER 20MIN	17.8										
AFTER 30MIN	18.4										
<p>Graph 8 shows the temperature of ambient are measured at four stages 1. Initial temp 2. After 10 minutes 3. After 20 minutes 4. After 30 minutes.The initial temperature of ambient, at initial condition the temp is 28.8,after 10 minutes the temp is 32.3,after 20 minutes the temp is 32.7 and after 30 minutes the temp is 34.1.</p>	 <table border="1"> <caption>AMBIENT</caption> <thead> <tr> <th>Condition</th> <th>Temperature</th> </tr> </thead> <tbody> <tr> <td>INITIAL</td> <td>28.8</td> </tr> <tr> <td>AFTER 10MIN</td> <td>32.3</td> </tr> <tr> <td>AFTER 20MIN</td> <td>32.7</td> </tr> <tr> <td>AFTER 30MIN</td> <td>34.1</td> </tr> </tbody> </table>	Condition	Temperature	INITIAL	28.8	AFTER 10MIN	32.3	AFTER 20MIN	32.7	AFTER 30MIN	34.1
Condition	Temperature										
INITIAL	28.8										
AFTER 10MIN	32.3										
AFTER 20MIN	32.7										
AFTER 30MIN	34.1										
<p>Graph 9 shows the temperature of evaporator out are measured at four stages 1. Initial temp 2. After 10 minutes 3. After 20 minutes 4. After 30 minutes.The initial temperature of evaporator out is, at initial condition the temp is 28.9,after 10 minutes the temp is 16.7,after 20 minutes the temp is 17.1 and after 30 minutes the temp is 17.8.</p>	 <table border="1"> <caption>EVAPORATOR OUT</caption> <thead> <tr> <th>Condition</th> <th>Temperature</th> </tr> </thead> <tbody> <tr> <td>INITIAL</td> <td>28.9</td> </tr> <tr> <td>AFTER 10MIN</td> <td>16.7</td> </tr> <tr> <td>AFTER 20MIN</td> <td>17.1</td> </tr> <tr> <td>AFTER 30MIN</td> <td>17.8</td> </tr> </tbody> </table>	Condition	Temperature	INITIAL	28.9	AFTER 10MIN	16.7	AFTER 20MIN	17.1	AFTER 30MIN	17.8
Condition	Temperature										
INITIAL	28.9										
AFTER 10MIN	16.7										
AFTER 20MIN	17.1										
AFTER 30MIN	17.8										

Ozone Layer Depletion Concerns

Montreal Protocol an international conference held in Montreal in September 1987, both developed and developing countries decided to control the production of Ozone Depletion Substance (ODS). As CFCs and HFCs are mainly effecting the ozone layer and depleting them from earth’s atmosphere.

Kyoto Protocol concentrated on the Global Warming impacts, this protocol was noticed by the third conference of United Nations framework convention on climate change (UNFCCC) held in December 1997 at Kyoto. Due to high amount of production and consumption of HFCs and CFCs the earth’s temperature is increasing and it is predicted that average global rise in temperature from 1.4⁰C to 5.8⁰ C



III. CONCLUSION

The main drawback of R-22 is that it has more Ozone layer Depletion and more Global Warming Potential than R134a. And the theoretical properties of R134a are more reliable and Coefficient of Performance is more than R134a. Based on the Montreal & Kyoto, Reliability, Economical wise R134a is best alternative substitute of R22

REFERENCES

- [1] Refrigeration and air conditioning by R S Khurmi
- [2] Websites: airconditioning-systems.com, samsung.com, air-conditioning-and-refrigeration-guide.com, air-conditioning-and-refrigeration-guide.com, wakefree.com
- [3] Atkinson, K.N., Drakulic, R., Heikal, M.R., Cowell, T.A., 1998, "Two and three dimensional numerical models of flow and heat transfer over louvered fin arrays in compact heat exchangers", International Journal of Heat and Mass Transfer, Vol. 41, pp. 4063-4080.
- [4] Coulomb, D., 2006, "Refrigeration: The challenges associated with sustainable development", Proceedings of the 6th International Conference on Compressors and Coolants, Slovak Republic, CD-ROM
- [5] Ereke, A., Özerdem, B., Bilir, L., Ilken, Z., 2005, "Effect of geometrical parameters on HT and pressure drop characteristics of plate fin and tube heat exchangers", App. Thermal Engg, Vol. 25, pp. 2421-2431.
- [6] Jang, J.Y., Wu, M.C., Chang, W. J., 1996, "Numerical and experimental studies of three-dimensional plate fin and tube heat exchangers", International Journal of Heat and Mass Transfer, Vol. 39, pp. 3057-3066.
- [7] Kays, W.M., London, A.L., 1998, "Compact Heat Exchangers", 3rd Ed., Krieger, Malabar, FL. 335 p.
- [8] Kim, Y., Tikhonov, A., Shin, Y., Lee, J., 2006, "Experimental study on high performance defrosting heater for household refrigerator", Proceedings of the 13th International H T Conference, Sydney, Australia, Aug.13-18.
- [9] Lee, T.-H., Lee, J.-S., Oh, S.-Y., Lee, M.-Y., Lee, K.-S., 2002, "Comparison of air-side heat transfer coefficients of several types of evaporators of household freezer/refrigerators", Proceedings of the 9th International Refrigeration and Air Conditioning Conference at Purdue, West Lafayette, IN, July 16-19.
- [10] Leu, J.S., Liu, M.S., Liaw, J.S., Wang, C.C., 2001, "A numerical investigation of louvered fin-and-tube heat exchangers having circular and oval tube configurations", I J H & M T Vol. 44, pp. 4235-4243.
- [11] Melo, C., Piucco, R.O., Duarte, P.O.O., 2006, "In-situ performance evaluation of no-frost evaporators", Proceedings of the 11th International R & A C Conference at Purdue, West Lafayette, IN, July 17-20.
- [12] Shih, T.-H., Liou, W.W., Shabbir, A., Yang, Z. and Zhu, J., 1995, "A new eddy-viscosity model for high Reynolds number turbulent flows - Model development and validation", Computers and Fluids, Vol. 24, pp. 227-238.
- [13] Shih, Y.C., 2003, "Numerical study of heat transfer performance on the air side of evaporator for a domestic refrigerator", Numerical Heat Transfer, Part A, Vol. 44, pp. 851-870.
- [14] Van Doormaal, J.P. and Raithby, G.D., 1984, "Enhancements of the SIMPLE method for predicting incompressible fluid flows", Numerical Heat Transfer, Vol. 7, pp. 147-163.
- [15] Waltrich, P.J., 2008, "Analysis & Optimization of Accelerated Flow Evaporators for Household Refrigeration Applications" (in Portuguese), MSc thesis, Federal University of Santa Catarina, Florianópolis, SC, Brazil.
- [16] U N Environmental Program, Montreal protocol on substance that deplete the ozone layer. Final act New York (1987).
- [17] Zaghdoudi, M.C., S.Maalej, Y.Saad and M.Bouchaala, A comparative study on the Performance and Environmental characteristics of Alternatives to R22 in residential Air Conditioners for Tunisian Market, Journal of Environmental Science and Engineering, Volume 4, No.12 (2010).
- [18] Devotta S., Waghmare A.V., Sawant N.N and Domkundwar B.M Alternatives to HCFC-22 for air conditioners applied Thermal Engineering, Volume 21 (2001) pp703-715.
- [19] Domanski P.A and Didion D.A, Thermodynamic Evaluation of R-22 alternative refrigerants and refrigerant mixtures Aahrae Transactions 99 (1993) pp636-648 part 2.
- [20] Chen S, Groll R & Rantermacher R., Theoretical analysis of HC refrigerant mixtures as a replacement for HCFC-22 for residential uses, Prucurtings of 1994 International Refrigeration conference at Purdue, Purdue University, West Lafayette, Indiana, USA (1994), pp225-230S. Venkataiah., G. Venkata Rao., A comparative study of the performance characteristics of alternative refrigerants to R-22 in room Air Conditioners. International Journal of Engineering Research and Technology Volume 6, Number 3, page no.333-343 (2013).
- [21] S. Venkataiah., G. Venkata Rao, Performance Evaluation of R-22 refrigerant at various Evaporating temperatures. 4th National Conference on Advance in Mech. Engineering 7th- 8th November 2013 pp 210-214.
- [22] NIST REFPROP- Thermodynamic and transport properties of refrigerants and refrigerant mixtures, standard Reference database reference 23- version 6.01. National Institute of Technology, Gaithersburg, MD.
- [23] Cool Pack Version 1.49 Refrigeration and Air Conditioning Simulation tool.